

VILNIUS UNIVERSITY
CENTER FOR PHYSICAL SCIENCES AND TECHNOLOGY

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NEW MATERIALS FOR ALKALINE FUEL CELLS: SYNTHESIS,
CHARACTERIZATION AND PROPERTIES

Summary of doctoral dissertation

Physical Sciences, Chemistry (03 P)

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The dissertation has been prepared at the Department of Catalysis of Center for Physical Sciences and Technology during the period of 2012 - 2016.

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VILNIAUS UNIVERSITETAS
FIZINIŲ IR TECHNOLOGIJOS MOKSLŲ CENTRAS

ALDONA BALČIŪNAITĖ

**NAUJOS MEDŽIAGOS ŠARMINIAMS KURO ELEMENTAMS: SINTEZĖ,
CHARAKTERIZAVIMAS IR SAVYBĖS**

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1. INTRODUCTION

The thesis is related to the search of new effective materials, that can be used for development and design of direct borohydride fuel cells (DBFCs) in order to improve the performance of existing fuel cells or create novel fuel cells with high efficiency. The fuel cell is a device that converts the chemical reaction energy (e.g., oxidation of fuel) directly into electricity. Fuel cells are well-known as the cleanest method for energy production, because water is formed as a by-product, which does not pollute the environment.

The AuM (M = Ni, Co, Cu) catalysts deposited on the titanium (Ti) or titania nanotube arrayed (TiO₂-NTs) surfaces were fabricated by means of simple and low-cost electrochemical, electroless metal deposition and galvanic displacement techniques. The created catalysts are novel and promising materials that can be used as anodes in direct borohydride fuel cells.

Development of renewable energy resources is important in order to reduce dependence on imported fuel. The rapid development of renewable energy sources and the capability of local energy generation has been growing in Lithuania in recent years.

The aim of the work was

Fabrication of efficient catalysts, their characterization and application for direct borohydride fuel cells.

The main tasks of the work were as follows:

1. Preparation of the Au(M)/Ti and Au(M)/TiO₂-NTs (M=Ni, Cu, Co) catalysts using the electroless metal deposition and galvanic displacement techniques.
2. Characterization of the surface morphology, structure and composition of the Au(M)/Ti and Au(M)/TiO₂-NTs catalysts by means of field emission scanning electron microscopy (FESEM), X-ray diffraction (XRD) and inductively coupled plasma optical emission spectroscopy (ICP-OES).

3. Determination of electrocatalytic properties of the Au(M)/Ti and Au(M)/TiO₂-NTs catalysts towards the electrooxidation of sodium borohydride using electrochemical methods.

Defensive statements:

1. Efficient AuM (M = Ni, Cu, Co) catalysts can be deposited on the Ti and TiO₂-NTs surfaces by means of the electroless metal deposition and galvanic displacement techniques.

2. The prepared Au(M)/Ti and Au(M)/TiO₂NT (M = Ni, Cu, Co) catalysts are electrocatalytically active with respect to the electrooxidation of sodium borohydride and are suitable for applying them as the anodes in direct borohydride fuel cells.

3. The Au(M)/Ti and Au(M)/TiO₂-NTs (M = Ni, Cu, Co) catalysts exhibit a significantly higher electrocatalytic activity towards the electrooxidation of sodium borohydride as compared with that of pure Au, M/Ti or M/TiO₂-NTs catalysts.

Novelty and actuality of the work

This thesis is related to the intensively developing research in the field of fuel cells and nanomaterials. The methodology for fabrication of the Au(M)/Ti and Au(M)/TiO₂-NTs (M = Ni, Cu, Co) catalysts with low Au loadings has been established. This methodology establishes sound scientific bases for developing efficient Au(M)/Ti and Au(M)/TiO₂-NTs catalysts with a significantly higher electrocatalytic activity towards the electrooxidation of sodium borohydride as compared to that of pure Au, M/Ti and M/TiO₂-NTs electrodes.

The novel catalysts, not used earlier, have been proposed for the oxidation of sodium borohydride. The highest electrocatalytic activity with respect to the electrooxidation of sodium borohydride has been obtained on the Au(Co)/Ti catalysts.

The prepared catalysts were applied as anode materials in the direct alkaline NaBH₄-H₂O₂ single fuel cell. These catalysts exhibit higher performance than the previously used catalysts in direct borohydride fuel cells. It has been found that these Au(M)/Ti and Au(M)/TiO₂-NTs catalysts can be successfully used in practical fuel cells as anodes.

2. EXPERIMENTAL

Chemicals. Titanium foil (99.7% purity, 0.127 mm thick), H₂SO₄ (95%), NH₄F (98%), PdCl₂ (59.5% Pd), C₂H₅OH (96%), NiSO₄·6H₂O (99%), C₂H₅O₂N (99%), NaH₂PO₂·H₂O (97%), Na₂C₃H₂O₄ (98%), CuCl₂·2H₂O (99%), CoCl₂·6H₂O (98%), C₄H₁₃N₃ (99%), CoSO₄·7H₂O, (99.5%), C₄H₁₂BNO (97%), HAuCl₄·3H₂O (99.9% Au), HCl (35-38%), NaBH₄ (96%) and NaOH (98.8%) were purchased from Sigma-Aldrich Supply. All chemicals were of analytical grade. Deionized (Elix 3 Millipore) water was used to prepare the electrolyte solutions. A Nafion N117 membrane was purchased from DuPont (Wilmington, DE).

Fabrication of catalysts. The self-ordered titania nanotube arrays (TiO₂-NTs) were prepared by anodic oxidation of Ti foil surface. Briefly, prior to anodization, titanium sheets (1 cm × 1 cm) were degreased with ethanol, rinsed with deionized water and dried in an Ar stream. Anodization of Ti sheets was performed in a 0.24 M H₂SO₄ solution with 0.5 wt.% NH₄F at a constant potential of 20 V at room temperature for 1 h. Two sheets of Pt were used as counter electrodes.

The M/Ti and M/TiO₂-NTs catalysts were prepared according to the following procedures: (i) activation of the Ti or TiO₂-NTs electrodes in a 1.7 mM PdCl₂ acidic solution for 60 s; (ii) subsequent rinsing of the activated surfaces with deionized water; (iii) followed by the immersion of the activated samples into the electroless Ni, Co or Cu plating baths. The Ni plating bath consists of 0.1 M NiSO₄, 0.4 M C₂H₅O₂N, 0.25 M NaH₂PO₂ and 0.1 M C₃H₂O₄Na₂. The bath operated at pH 9 and at a temperature of 85 °C for 1 min.

The Co plating bath consisted of 0.05 M NiSO₄, 0.015 M diethylenetriamine and 0.05 M borane morpholine complex. The bath operated at pH 7 and at a temperature of 25 °C for 45 min.

The Cu plating bath consisted of 0.05 M CuCl₂, 0.15 M CoCl₂ and 0.6 M diethylenetriamine. The bath operated at pH 6 and at a temperature of 20 °C for 10 min.

The electroless Co and Cu plating baths were purged with Ar to remove air oxygen.

The Au crystallites were deposited on the prepared M/Ti or M/TiO₂-NTs electrodes by their immersion into 1 mM HAuCl₄ + 0.1 M HCl (denoted as Au(III)-containing solution) for 0.5, 1 and 5 min.

Characterization of catalysts. The surface morphology and composition of the fabricated catalysts were characterized using a SEM/FIB workstation Helios Nanolab 650 with an energy dispersive X-ray (EDX) spectrometer INCA Energy 350 X-Max 20.

The Au metal loading in the prepared catalysts was estimated using an ICP optical emission spectrometer Optima 7000DV (Perkin Elmer) at wavelengths of $\lambda = 267.595$ and 242.795 nm. For calibration, the standard solutions of 1.0 and 10.0 mg l⁻¹ were used (Perkin Elmer).

XRD patterns of the prepared catalysts were measured using an X-ray diffractometer SmartLab (Rigaku) equipped with an 9 kW X-ray tube with a rotating Cu anode. The grazing incidence (GIXRD) method was used in the 2Θ range 35 – 80°. The angle between the parallel beam of X-rays and a specimen surface (ω angle) was adjusted to 0.5°.

Electrochemical measurements. Electrochemical measurements were performed with a Metrohm Autolab potentiostat (PGSTAT100) using a conventional three-electrode electrochemical cell. The M/Ti, M/TiO₂-NTs, Au(M)/Ti and Au(M)/TiO₂-NTs catalysts with a geometric area of 2 cm² were employed as working electrodes, an Ag/AgCl/KCl_{sat} electrode was used as reference and a Pt sheet was used as a counter electrode. An Au-sputtered quartz crystal with a geometric area of 0.636 cm² was used as a bare Au electrode.

The electrochemically active areas of Au surface (ESAs) in the catalysts were determined from the cyclic voltammograms of bare Au, Au(M)/Ti and Au(M)/TiO₂-NTs catalysts recorded in a deaerated 0.5 M H₂SO₄ solution at a scan rate of 50 mV s⁻¹. The ESAs of Au nanoparticles in the catalysts were calculated by the charge associated with the Au surface oxide reduction peak (400 μ C cm⁻² for a monolayer) [3].

Sodium borohydride oxidation was investigated by recording cyclic voltammograms (CVs) in a 1 M NaOH solution containing 0.05 M NaBH₄ at a potential scan rate of 10 mV s⁻¹ from the open circuit potential values in the anodic direction up to 0.6 V vs. Ag/AgCl/KCl_{sat} at a temperature of 25 °C. The chronoamperometric curves for the M/Ti,

M/TiO₂-NTs, Au(M)/Ti and Au(M)/TiO₂-NTs catalysts were recorded at a constant potential values for 2 min.

Fuel cell test experiments. Direct borohydride-hydrogen peroxide fuel cell (DBHPFC) tests were carried out by employing the M/Ti, M/TiO₂-NTs, Au(M)/Ti and Au(M)/TiO₂-NTs catalysts (with a geometric area of 2 cm²) as the anode and a Pt sheet with a geometric area of 6 cm² as the cathode. Each compartment of the cell contained 100 mL of the corresponding aqueous electrolyte. The anolyte was composed of an alkaline mixture of 1 M NaBH₄ + 4 M NaOH and the catholyte containing 5 M H₂O₂ + 1.5 M HCl. To prevent H₂O₂ decomposition and possible loss of BH₄⁻ by hydrolysis during storage, the test solutions were prepared immediately before the measurements. A Nafion[®] N117 membrane was used to separate the anodic and cathodic compartments of the single direct NaBH₄-H₂O₂ fuel cell. The active area of membrane was ca. 30 cm². Cell measurements were conducted using a Zennium electrochemical workstation (ZAHNER-Elektrik GmbH & Co. KG). The performance of the fuel cell was evaluated by recording the cell polarization and obtaining the corresponding power density curves.

3. RESULTS AND DISCUSSIONS

3.1 Characterization of catalysts

The Au(M)/Ti and Au(M)/TiO₂-NTs (M = Ni, Co, Cu) catalysts were prepared by partial galvanic displacement of electroless metal layers, deposited on the Ti and TiO₂-NTs surfaces, by Au nanoparticles from the Au(III)-containing solution.

Self-ordered TiO₂ nanotube arrays in this study were prepared by anodic oxidation of Ti surface in an aqueous sulfuric acid solution containing NH₄F. The average tube diameter was ca. 100 nm and the thickness of titania nanotubes was ~310 nm (Fig. 1).

The electroless Ni layer with the thickness of ca. 300 nm was deposited on the titanium and titania nanotube surfaces, which produces a layer of granular nickel crystallites ca. 200 nm in size (Fig. 2 a,b). The data of EDX analysis are given in Table I. It should be noted that the nickel layer is deposited on the Ti or TiO₂-NTs surfaces in the electroless

plating solution using sodium hypophosphite as a reducing agent. So, about 9 at.% of phosphorus is co-deposited with Ni.

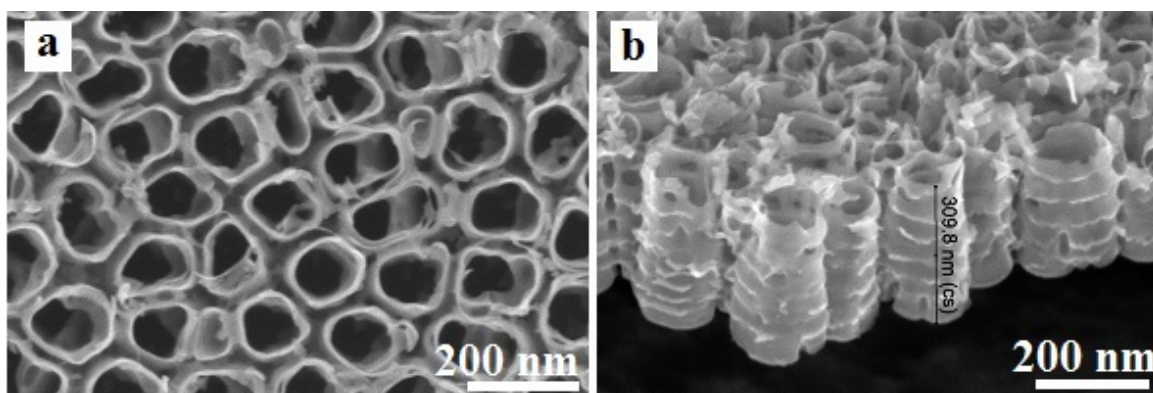


Fig. 1. SEM micrographs of top side (a) and cross-sectional side view (b) of as-prepared TiO_2 -NTs.

TABLE I. The contents of elements on the surface of the Ni/Ti and Ni/ TiO_2 -NTs electrodes by EDX analysis. The catalysts are the same as in Figure 2 (a,b).

Catalysts	Elements, at.%				Size of crystallites, μm
	Ni	P	O	Ti	
Ni/Ti	62.73	9.39	8.13	19.93	0.2
Ni/ TiO_2 -NTs	79.65	8.40	2.96	8.99	0.2

The layers of polycrystalline Co with average crystallites size of ca. 400-900 nm and 400-1000 nm and the thickness of ca. 1.1 μm were deposited on the Ti and TiO_2 -NTs surfaces, respectively (Fig. 2 c,d). The data of EDX analysis are shown in Table II.

TABLE II. The contents of elements on the surface of the Co/Ti and Co/ TiO_2 -NTs catalysts by EDX analysis. The catalysts are the same as in Figure 2(c,d).

Catalysts	Elements, at.%			Size of crystallites, μm
	Co	O	Ti	
Co/Ti	34.82	24.41	40.78	0.4-0.9
Co/ TiO_2 -NTs	66.16	21.17	12.67	0.4-1

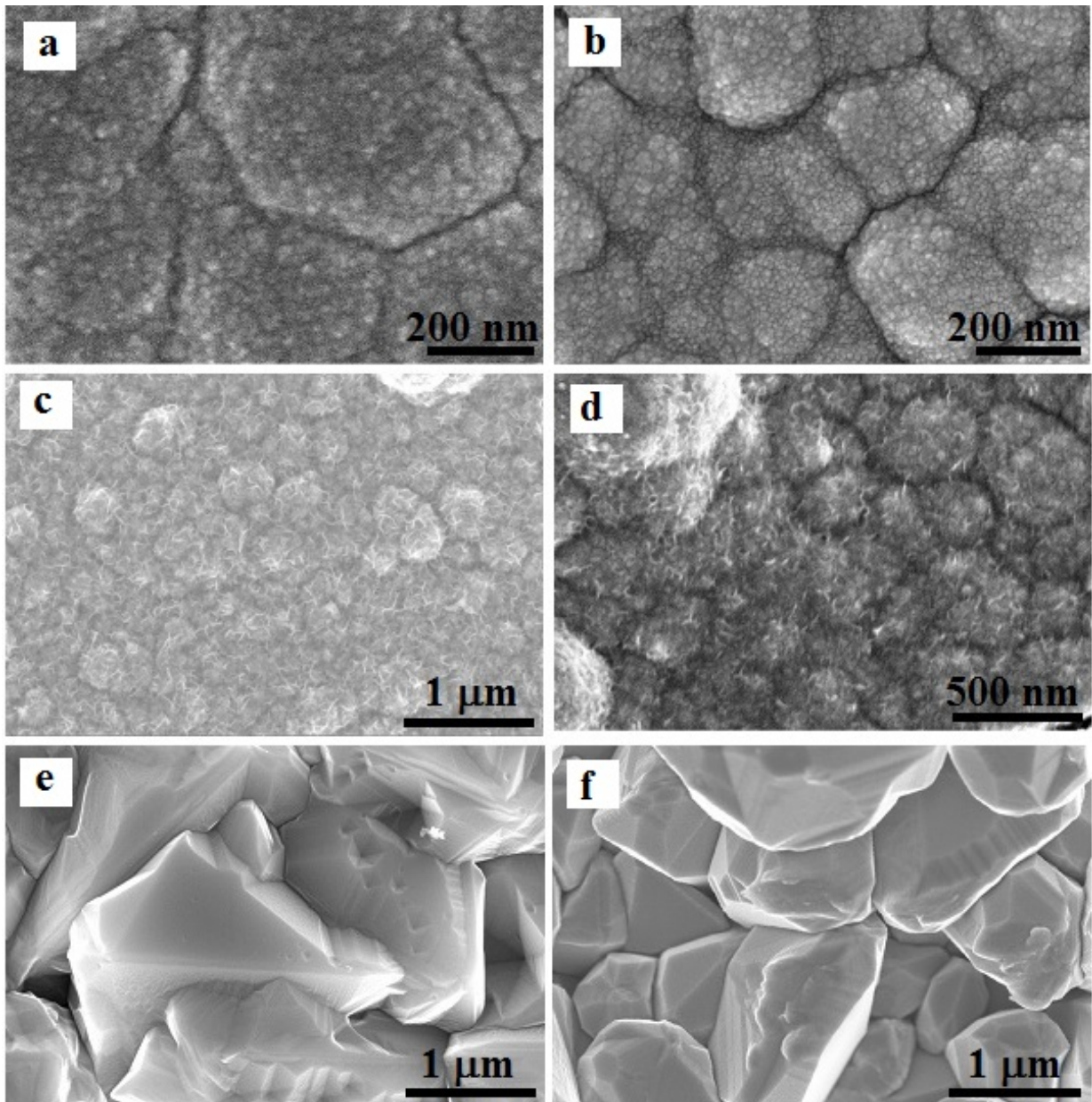


Fig. 2. SEM micrographs of the top side views of as-prepared Ni/Ti (a), Ni/TiO₂-NTs (b) Co/Ti (c), Co/TiO₂-NTs (d), Cu/Ti (e) and Cu/TiO₂-NTs (f). The M/Ti and M/TiO₂-NTs catalysts were prepared by immersion of Ti or TiO₂-NTs into the Ni plating bath at 85 °C for 1 min (a,b), Co plating bath at 25 °C for 45 min (c,d) and Cu plating bath at 20 °C for 10 min (e,f).

The layers of polycrystalline Cu with the average size of crystallites of ca. 1 μm and the thickness of ca. 1.5 μm were deposited on the Ti and TiO₂-NTs surfaces (Fig. 2 e,f). The data of EDX analysis of the as-prepared catalysts are given in Table III.

TABLE III. The contents of elements on the surface of the Cu/Ti and Cu/TiO₂-NTs catalysts by EDX analysis. The catalysts are the same as in Figure 2 (e,f).

Catalysts	Elements, at.%			Size of crystallites, μm
	Cu	O	Ti	
Cu/Ti	97.74	1.24	1.02	1
Cu/TiO ₂ -NTs	94.93	2.33	2.74	1

The Au nanoparticles were deposited on the M/Ti or M/TiO₂-NTs surfaces by galvanic displacement. Immersion of the M/Ti or M/TiO₂-NTs surfaces into 1 mM HAuCl₄ + 0.1 M HCl for 0.5, 1 and 5 min results in deposition of Au crystallites on the surface of M/Ti or M/TiO₂-NTs. The SEM views of prepared Au(M)/Ti and Au(M)/TiO₂-NTs catalysts are presented in Figs. 3-5. The Au nanoparticles of ca. 10-50 nm and 10-30 nm in size were deposited on the Ni/Ti (Fig. 3a-c) and Ni/TiO₂-NTs (Fig. 3d-f) electrodes, respectively, after their immersion into the Au(III)-containing solution for 0.5, 1 and 5 min (Fig. 3). The Au crystallites appear as bright spots and they are quite uniform in size and well separated (Fig. 3).

As evident from Fig. 4, the Au crystallites of the cubic shape and homogeneously dispersed were deposited on the Co/Ti (Fig. 4a-c) and Co/TiO₂-NTs (Fig. 4d-f). After immersion of the Co/Ti and Co/TiO₂-NTs electrodes into the Au(III)-containing solution for 0.5, 1 and 5 min, the Au crystallites of ca. 15-100 nm and 10-75 nm in size were deposited on Co/Ti (Fig. 4a-c) and Co/TiO₂-NTs (Fig. 4d-f), respectively.

Immersion of the Cu/Ti and Cu/TiO₂-NTs electrodes in an Au(III)-containing solution for 0.5, 1 and 5 min, respectively, results in deposition of Au nanoparticles sized 10 to 50 nm (Fig. 5).

The summarized data of investigated Au(M)/Ti and Au(M)/TiO₂-NTs catalysts by EDX analysis are given in Table IV. The analysis of all prepared Au(M)/Ti and Au(M)/TiO₂-NTs catalysts confirms the presence of Au, Ni, Co and Cu on the Ti and TiO₂-NTs electrodes. In all cases, significant amounts of deposited Ni, Co or Cu and a much lower amount of Au were detected on the surface of catalysts (Table IV).

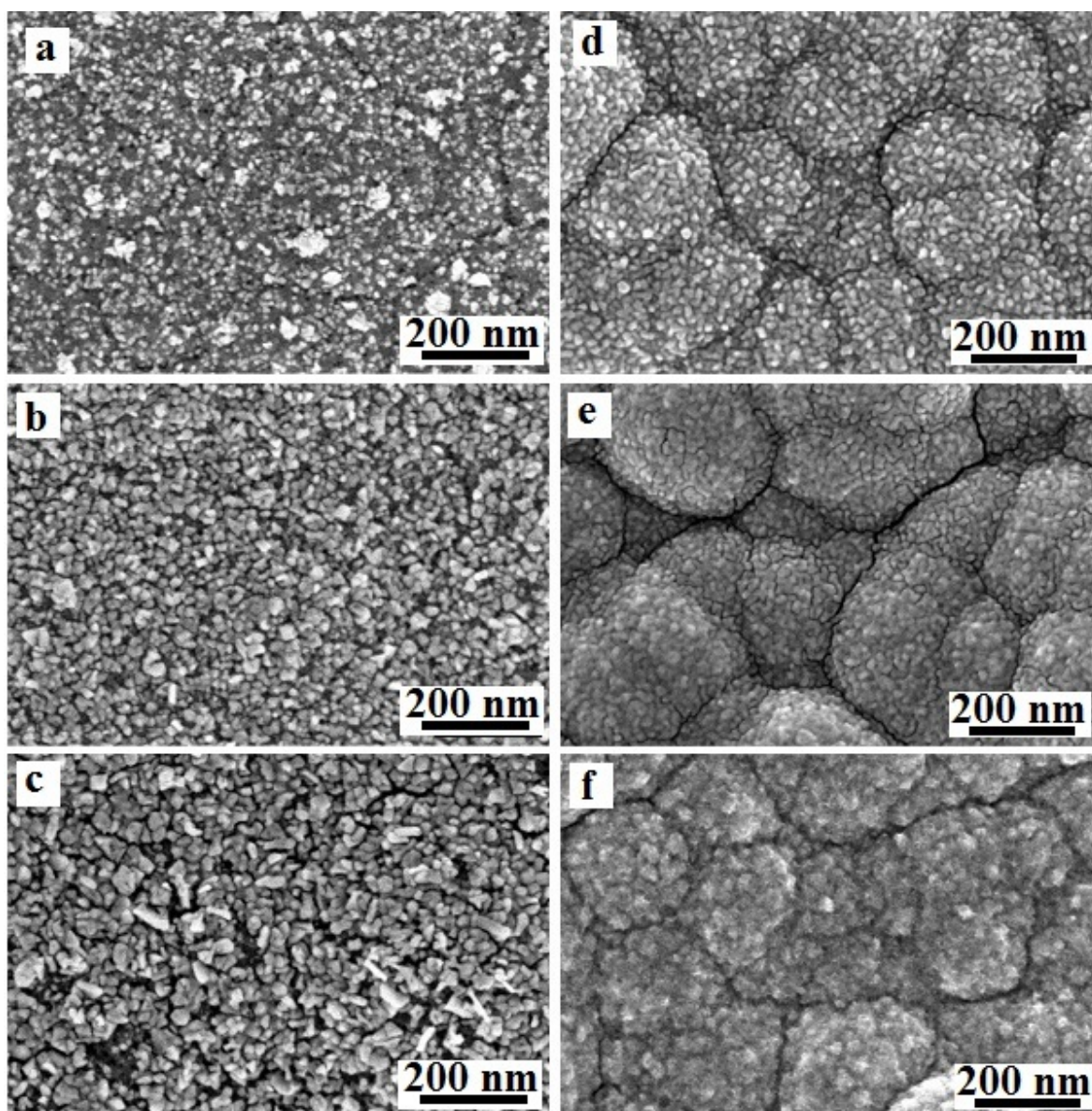


Fig. 3. SEM micrographs of top side views of as-prepared Au(Ni)/Ti (a-c) and Au(Ni)/TiO₂-NTs (d-f) catalysts. The catalysts were prepared by immersion of Ti or TiO₂-NTs into the Ni plating bath at 85 °C for 1 min, followed by their immersion in 1 mM HAuCl₄ + 0.1 M HCl at 25 °C for 0.5 (a,d), 1 (b,e) and 5 (c,f) min.

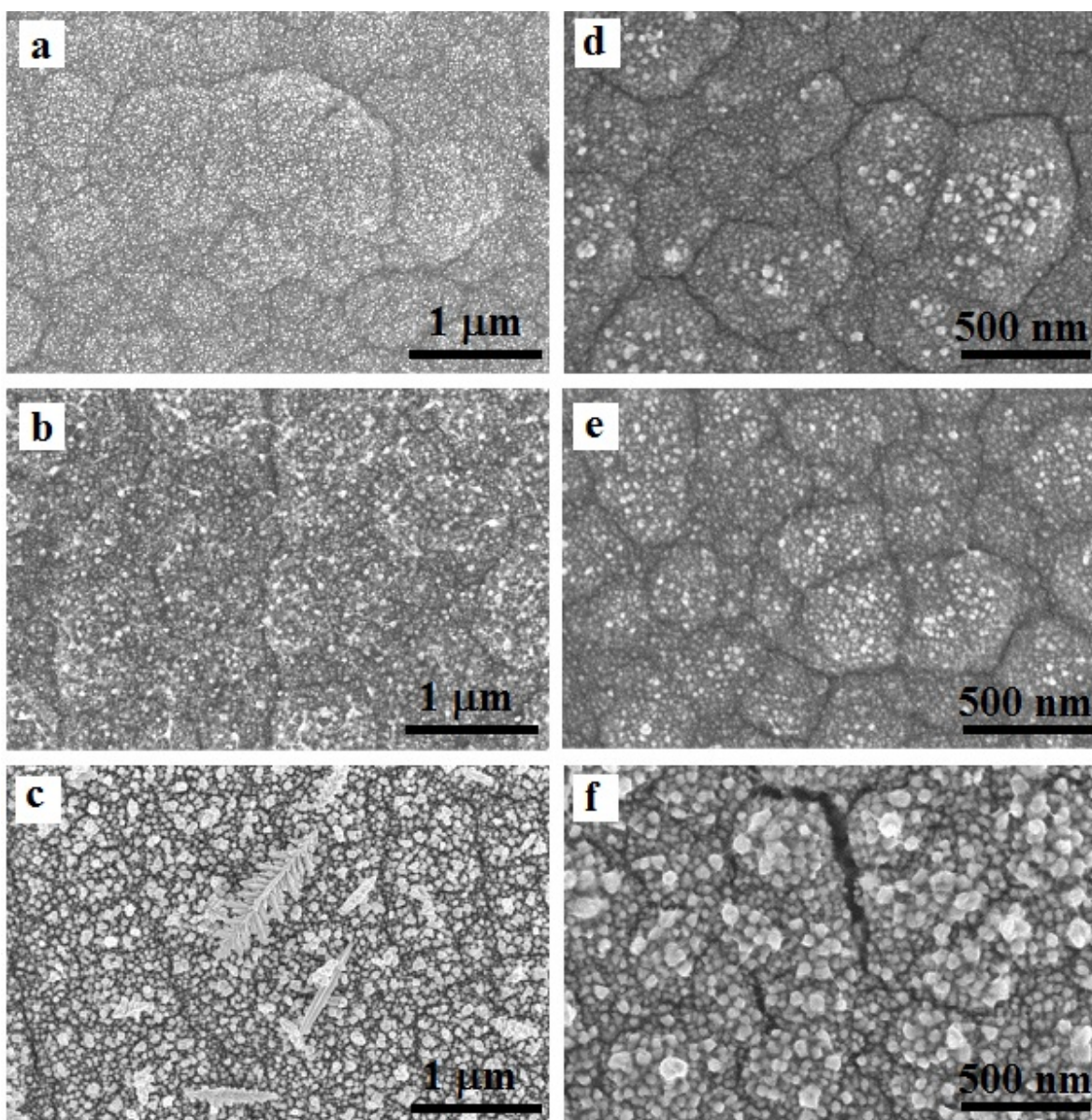


Fig. 4. SEM micrographs of top side views of as-prepared Au(Co)/Ti (a-c) and Au(Co)/TiO₂-NTs (d-f) catalysts. The catalysts were prepared by immersion of Ti or TiO₂-NTs into the Co plating bath at 25 °C for 45 min, followed by their immersion in 1 mM HAuCl₄ + 0.1 M HCl at 25 °C for 0.5 (a,d), 1 (b,e) and 5 (c,f) min.

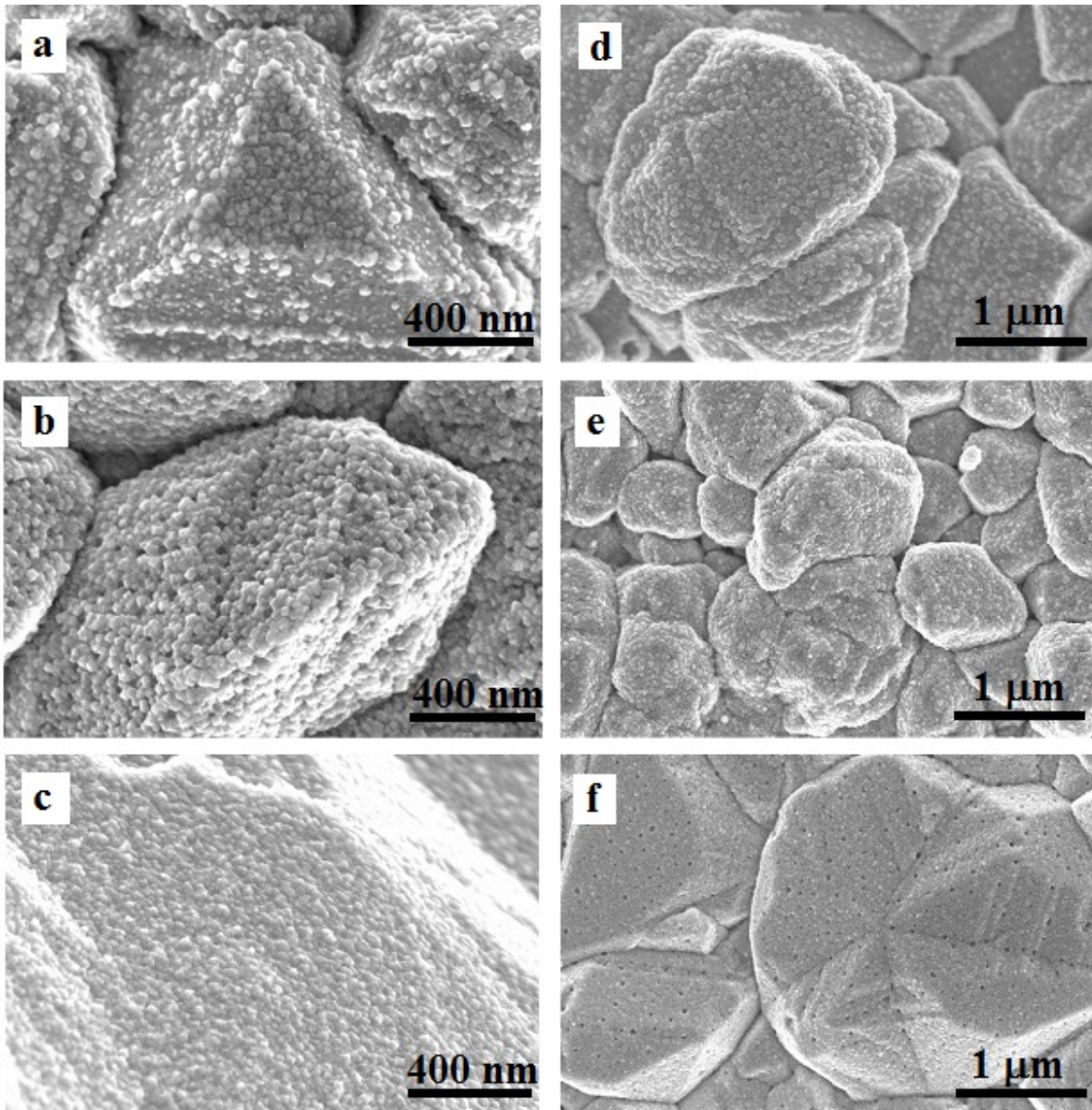


Fig. 5. SEM micrographs of top side views of as-prepared Au(Cu)/Ti (a-c) and Au(Cu)/TiO₂-NTs (d-f) catalysts. The catalysts were prepared by immersion of Ti or TiO₂-NTs into the Cu plating bath at 20 °C for 10 min, followed by their immersion in 1 mM HAuCl₄ + 0.1 M HCl at 25 °C for 0.5 (a,d), 1 (b,e) and 5 (c,f) min.

TABLE IV. The contents of elements on the surface of the Au(M)/Ti and Au(M)/TiO₂-NTs catalysts by EDX analysis. The catalysts are the same as in Figures 3, 4 and 5. The Au loadings were estimated from ICP-OES measurements.

Au(Ni)/Ti and Au(Ni)/TiO₂-NTs catalysts

Catalysts	Au deposition time, min	Elements, at. %					Particle size, nm	Au loading, $\mu\text{g cm}^{-2}$	ESA, cm^2
		Au	Ni	P	O	Ti			
Au(Ni)/Ti	0.5	0.23	51.47	7.46	2.69	38.14	10-30	0.9	3.3
	1	0.61	53.18	7.25	2.36	36.60	10-30	1.8	5.5
	5	1.29	46.00	5.12	4.64	42.95	10-50	8.4	6.6
Au(Ni)/TiO ₂ -NTs	0.5	0.34	73.86	5.18	3.22	17.41	10-30	8.2	1.3
	1	0.62	74.54	5.47	3.27	16.10	10-30	10.6	2.7
	5	1.38	71.56	5.65	3.98	17.44	10-30	34.1	4.2

Au(Co)/Ti and Au(Co)/TiO₂-NTs catalysts

Catalysts	Au deposition time, min	Elements, at. %				Particle size, nm	Au loading, $\mu\text{g cm}^{-2}$	ESA, cm^2
		Au	Co	O	Ti			
Au(Co)/Ti	0.5	0.22	54.60	31.86	13.32	15-50	4.2	0.7
	1	1.01	58.61	27.81	12.58	15-50	16.9	2.0
	5	2.86	27.80	48.34	21.01	30-100	57.6	6.9
Au(Co)/TiO ₂ -NTs	0.5	0.35	38.83	41.21	19.61	10-35	10.0	1.4
	1	0.51	32.50	49.55	17.44	10-40	22.2	2.2
	5	1.16	14.89	61.27	22.68	10-75	59.4	3.8

Au(Cu)/Ti and Au(Cu)/TiO₂-NTs catalysts

Catalysts	Au deposition time, min	Elements, at. %				Particle size, nm	Au loading, $\mu\text{g cm}^{-2}$	ESA, cm^2
		Au	Cu	O	Ti			
Au(Cu)/Ti	0.5	1.77	95.49	1.04	1.71	10-50	5.6	1.1
	1	2.73	94.67	1.27	1.34	10-50	9.8	3.9
	5	6.87	91.14	0.75	1.24	10-50	19.8	7.9
Au(Cu)/TiO ₂ -NTs	0.5	0.29	91.29	6.21	2.21	10-50	8.5	1.7
	1	0.46	88.03	6.39	5.13	10-50	11.3	2.2
	5	1.35	92.65	4.64	1.36	10-50	23.4	7.5

The Au metal loadings in the Au(M)/Ti and Au(M)/TiO₂-NTs catalysts were determined by means of inductively coupled plasma optical emission spectroscopy and are given in Table IV. It has been determined that the Au loadings were 0.9, 1.8 and 8.4 $\mu\text{g}_{\text{Au}} \text{cm}^{-2}$ and 8.2, 10.6 and 34.1 $\mu\text{g}_{\text{Au}} \text{cm}^{-2}$ in the fabricated Au(Ni)/Ti and Ni/TiO₂-NTs, respectively, catalysts after sonication of the Ni/Ti and Ni/TiO₂-NTs electrodes in an Au(III)-containing solution for 0.5, 1 and 5 min, respectively.

After immersion of the Co/Ti and Co/TiO₂-NTs electrodes into the Au(III)-containing solution for 0.5, 1 and 5 min, the Au nanoparticles with the Au loadings of 4.2, 16.9, 57.6 $\mu\text{g}_{\text{Au}} \text{cm}^{-2}$ and 10, 22, 59 $\mu\text{g}_{\text{Au}} \text{cm}^{-2}$, respectively, were deposited on Co/Ti and Co/TiO₂-NTs.

Then the Cu/Ti and Cu/TiO₂-NTs electrodes were immersed in an Au(III)-containing solution for 0.5, 1 and 5 min, respectively, the Au(Cu)/Ti and Au(Cu)/TiO₂-NTs catalysts were prepared with the Au loadings of 5.6, 9.8, 19.8 $\mu\text{g}_{\text{Au}} \text{cm}^{-2}$ and 8.5, 11.3, 23.4 $\mu\text{g}_{\text{Au}} \text{cm}^{-2}$, respectively (Table IV).

The electrochemically active areas of the surface of Au nanoparticles (ESA) in the catalysts were determined from the cyclic voltammograms of the Au, Au(M)/Ti and Au(M)/TiO₂-NTs catalysts recorded in a deaerated 0.5 M H₂SO₄ solution at a scan rate of 50 mV s⁻¹ by calculating the charge associated with Au oxide reduction (400 $\mu\text{C cm}^{-2}$ for a monolayer). The data obtained are given in Table IV. It should be noted that the ESA of pure Au electrode was 1.6 cm². The results show that the ESAs values of the catalysts prepared by immersion of M/Ti and M/TiO₂-NTs in an Au(III)-containing solution for 1 and 5 min, respectively, are ca. 2-5 times higher than those of pure Au.

Figure 6 a shows XRD patterns for the Ni/TiO₂-NTs (lower black colour pattern) and Au(Ni)/TiO₂-NTs catalysts prepared by immersion of Ni/TiO₂-NTs in a 1 mM HAuCl₄ + 0.1 M HCl solution at 25 °C for 1 and 5 min (upper curves). The presented 2 Θ ranges contain sharp XRD peaks of the Ti substrate and broad ones of Ni 111, Au 111, Au 200 and Au 220 (in the inset). The XRD peak Au 111 overlaps with that of Ti 002 and peak Au 200 with that of Ni 111. The presence of the Au can be apparently evidenced by the inset of Fig. 6 a.

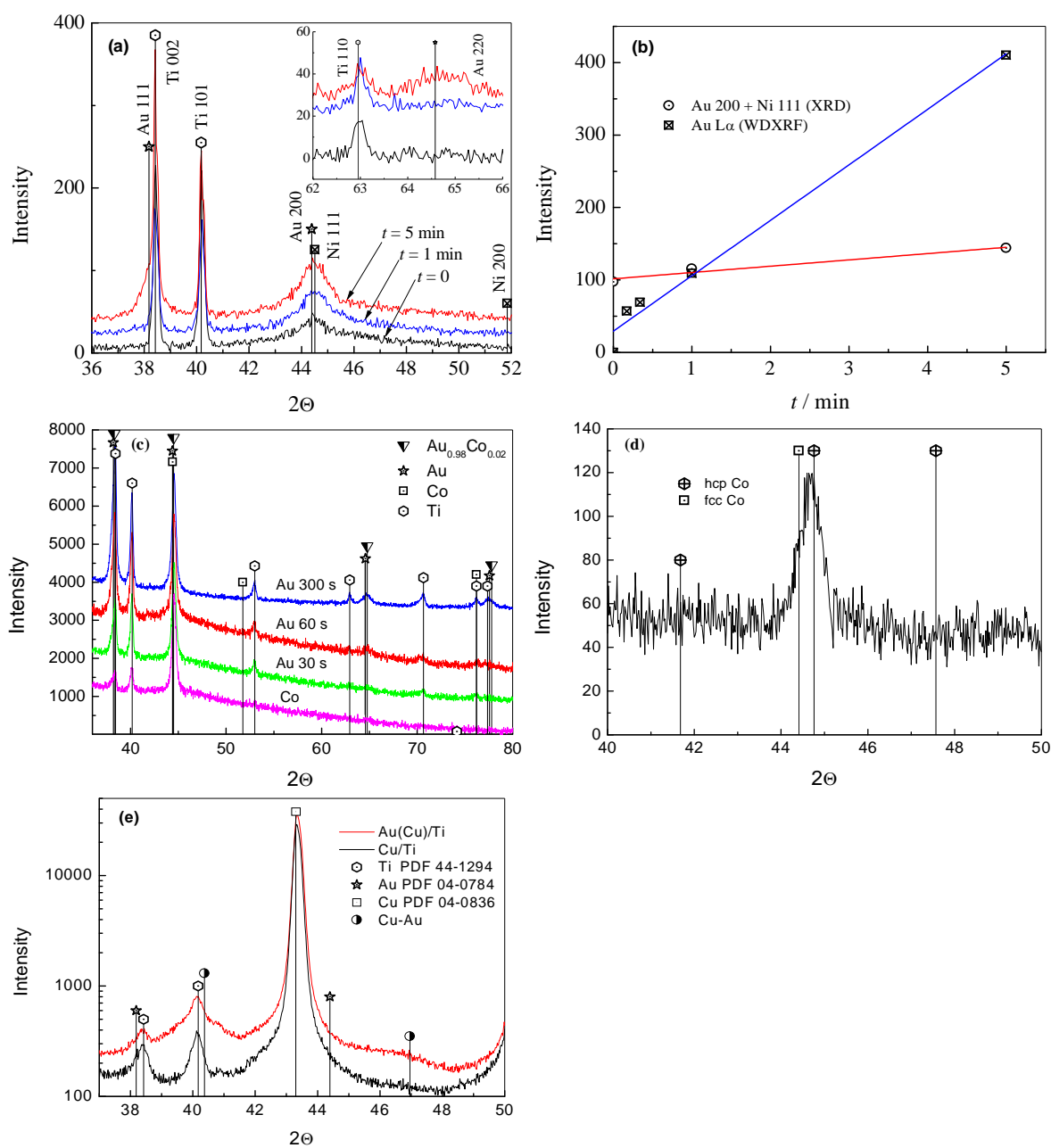


Fig. 6. XRD patterns: (a) Ni/TiO₂-NTs (lower black colour pattern) and Au(Ni)/TiO₂-NTs prepared by immersion of Ni/TiO₂-NTs in 1 mM HAuCl₄ + 0.1 M HCl at 25 °C for 1 and 5 min (upper curves); (b) The integral intensity of the overlapping XRD peaks Au 200 and Ni 111 and intensity Au Lα peak of the x-ray spectrum for Au layers with different deposition time; (c) Co/Ti and Au(Co)/Ti, the same as in Fig. 4 (a-c); (d) Co layer measured using the in-plane technique; (e) Cu/Ti (upper curve) and Au(Cu)/Ti prepared by immersion of Ti sheets in the Cu plating bath at 20 °C for 10 min, followed by its immersion in 1 mM HAuCl₄ + 0.1 M HCl at room temperature for 5 min.

The upper curve corresponding to Au(Ni)/TiO₂-NTs, when duration of Au deposition was 5 min ($t_{\text{Audep}} = 5$ min), shows a broad peak at the position of XRD peak Au 220 according to PDF No 04-0784. There is no peak at this position in the lower XRD patterns corresponding to Au(Ni)/TiO₂-NTs ($t_{\text{Audep}} = 1$ min) and Ni/TiO₂-NTs ($t_{\text{Audep}} = 0$ min), respectively. The presence of Au is also evidenced by a hump on the left shoulder of the XRD peak Ti 002 in the pattern (upper red curve) for the Au(Ni)/TiO₂-NTs ($t_{\text{Audep}} = 5$ min) catalyst. It was difficult to determine precisely the value of the lattice parameter of Au due to low intensity and broadening of the peaks, however, it may be suggested that the Au peaks were a little bit shifted towards higher diffraction angles. That points to the formation of Ni solid solution in gold. The presence of the Au layer can be supported by Fig. 6 b, which shows an integral intensity of the XRD peaks Au 200 and Ni 111 as a function of Au deposition time. Since the thickness of Ni layer was always the same, the increase in the integral intensity of the overlapping peaks Au 200 and Ni 111 must be related with the increase in thickness of Au layer. Fig. 6 b also presents results of WDXRF measurements, i.e. the intensity of the Au L α peak of characteristic X-ray spectrum for the Au layers obtained at the Ni/TiO₂-NTs substrate at different deposition periods, which also supported the increase in thickness of the Au layer.

Figure 6 c shows XRD patterns for Co/Ti (lower curve) and Au(Co)/Ti prepared by immersion of Co/Ti in 1 mM HAuCl₄ + 0.1 M HCl for different periods (upper curves). The symbols indicate the positions of the XRD peaks of Ti (PDF card no 00-044-1294), Au (00-004-0784), Co (00-015-0806) and Au_{0.98}Co_{0.02} (04-001-1901). The lowest XRD pattern contains three XRD peaks of Ti substrate and only one strong peak attributable to Co. To ascertain which crystalline structure presents the cobalt layer – cubic face centered (fcc) structure or hexagonal (hcp) one, the XRD in-plane measurement was conducted since that enables to measure XRD peaks from crystallographic planes perpendicular to the sample surface. Figure 6 d shows the obtained XRD pattern, which evidences that there are no XRD peaks of the hcp structure, which does not overlap with the peak of fcc Co 111. However, XRD peak Co 111 is slightly shifted towards higher diffraction angles. Since Co was deposited using morpholine borane as a reducing agent, some amount of boron (in our case

up to 1 %) could be intercalated into the cobalt deposit; therefore, the above-mentioned shift could be explained by formation of a replacement solid solution of boron in cobalt.

Figure 6 e presents XRD patterns for Cu/Ti and Au(Cu)/Ti prepared by immersion of Cu/Ti electrode in a 1 mM H₂AuCl₄ + 0.1 M HCl solution at 25 °C for 5 min (upper curve). The presented 2 θ ranges contain XRD peaks: 100 and 002 of the Ti substrate and a strong peak 111 of Cu in the case of Cu/Ti. When Au was deposited on the Cu layer, two broad additional peaks appeared at the diffractions angles of ~40 and ~47°. The maxima of the peaks corresponded to the positions of peaks 111 and 200 of an fcc crystalline structure with the lattice parameter of 0.3867 nm. It could be believed that these peaks are of fcc phase of a continuous solid solution of Au and Cu. According to the relationship of lattice parameters and composition in the disordered fcc phase in the Au-Cu system, the proportion of Au in the solid solution was determined and it approximately equalled to 45 at.%. The broad XRD peaks (FWHM = 1.25° for the peak with a maximum at 47°) of the solid solution pointed to a very thin layer of the Au-Cu phase. On the other hand, the broadening of the peaks could be also caused by the inhomogeneity of the composition of the Au-Cu solid solution.

3.2. Electrochemical characterization

The electrocatalytic activity of the prepared catalysts towards the oxidation of BH₄⁻ ions was evaluated by cyclic voltammetry. Fig. 7 shows the oxidation of BH₄⁻ ions on the bulk Au electrode in 1.0 M NaOH containing 0.05 M NaBH₄ at a temperature of 25°C with a scan rate of 10 mV s⁻¹. Broad peaks of the direct oxidation of BH₄⁻ for bulk Au are observed at a potential of ca. -0.4 V (anodic peaks **A**), which is attributed to the direct oxidation of BH₄⁻ ions. Wide oxidation waves that extend up to 0.4 V correspond to the oxidation of reaction intermediates on the partially oxidized Au surface. In the backward scan, sharp peaks **B** are observed at ca. 0.2 V followed by a plateau in the potential region from 0 to -0.6 V. These peaks are attributed to the oxidation of the adsorbed species such as BH₃OH⁻ or other borohydrides formed as an intermediate during the oxidation of the BH₄⁻ ion in the forward scan.

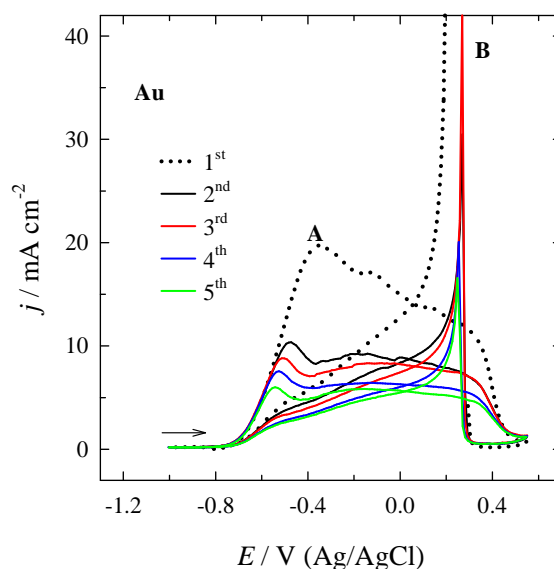


Fig. 7. CVs of bare Au in 0.05 M NaBH₄ + 1 M NaOH at 25 °C with a sweep rate of 10 mV s⁻¹.

The oxidation of borohydride was investigated on the Ni/Ti, Co/Ti and Cu/Ti electrodes by cyclic voltammetry. Figure 8 a presents the CVs for Ni/Ti in 1.0 M NaOH (*the inset a'*) and in that containing 0.05 M NaBH₄ at 25 °C with a scan rate of 10 mV s⁻¹.

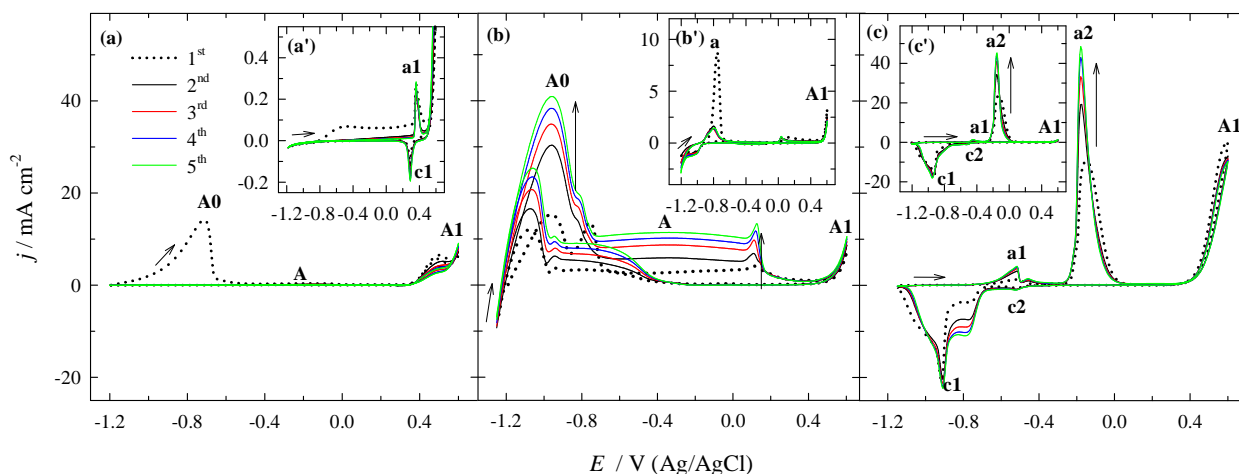


Fig. 8. Borohydride oxidation recorded on Ni/Ti (a), Co/Ti (b) and Cu/Ti (c) in 0.05 M NaBH₄ + 1 M NaOH at 10 mV s⁻¹; 25 °C. The insets represent the CVs of Ni/Ti (a'), Co/Ti (b') and Cu/Ti (c') recorded in 1 M NaOH.

As seen from the inset in Fig. 8 a', during the forward sweep, well-defined anodic (**a1**) and cathodic (**c1**) peaks are recorded. The peaks are associated with the transformation between β -Ni(OH)₂ and β -NiOOH. The anodic and cathodic potentials were at ca. 0.36 and 0.29 V. An addition of 0.05 M NaBH₄ to the 1.0 M NaOH solution (Fig. 8 a) results in anodic peak **A0** at more negative potential values at ca. -0.8 V. According to the literature, this peak is attributed to the oxidation of H₂, generated by the catalytic hydrolysis of BH₄⁻. At potentials higher than 0.4 V anodic peak **A1**, which corresponds to the oxidation reaction of Ni(OH)₂ → NiOOH is recorded, while the cathodic response of this reaction is not observed on the backward sweep. Hence, during the subsequent anodic scans no anodic peaks were observed at lower potential values. It may be proposed that the Ni layer deposited on the Ti surface does not catalyze the direct BH₄⁻ ions oxidation at higher potentials due to the passivation caused by nickel hydroxide(s) formation or, maybe, the surface of catalyst is poisoned by strongly adsorbed intermediates generated during the BH₄⁻ ion oxidation or sodium borohydride oxidation on the metal surface of Ni.

The borohydride oxidation on Co/Ti is shown in Figure 8 b. In the case of Co/Ti in 1 M NaOH (Fig. 8b, the inset b'), during anodic scan anodic peak **a** is observed at lower potential values. This anodic peak at ca. -0.8 V can be attributed to the formation of Co hydroxides/oxides in the alkaline medium at low potential values. The measured sodium borohydride oxidation current density values at Co/Ti are significantly greater as compared to those recorded in the background solution (1 M NaOH) at the latter catalyst (Fig. 8b). Two well-expressed anodic peaks **A0** and **A** are observed in the CVs recorded on the Co/Ti electrode in a 0.05 M NaBH₄ + 1 M NaOH solution. The measured oxidation current densities under the low-potential region from -1.2 to -0.7 V (peak **A0**) recorded on Co/Ti may be ascribed to the direct oxidation of borohydride anion. Based on the ground of FTIR, EQCM and RDDE investigations of the overall borohydride oxidation process on various catalysts show that the mechanism of borohydride oxidation is rather complicated due to the formation of intermediates, adsorption phenomenon and influence of electrode potential, e.g., formation, adsorption and oxidation of BH₃OH⁻. It may be assumed that in the low-potential region up to < -0.7 V borohydride oxidation on the Co/Ti electrode proceeds via

fully dissociative adsorption of BH_4^- . It was shown that in the low-potential region direct BH_4^- electrooxidation produces more electrons than the high-potential direct BH_4^- electrooxidation. In the case when potential values are more positive than 0.4 V, anodic peak **A1** is observed. This peak may be attributed to the formation of Co(III) surface compounds.

The electrochemical behavior of Cu/Ti electrode in the 1 M NaOH solution (the inset c') and in that containing 0.05 M NaBH_4 at a sweep rate of 10 mV s^{-1} is shown in Fig. 8 (c). The CVs recorded for the Cu/Ti electrode in both solutions are similar in shape except those at potential values higher than 0.4 V. Anodic peak **a1** at a potential value of -0.5 V is attributed to the formation of insoluble Cu(I) compounds and anodic peak **a2** at -0.25 V – to the formation of insoluble Cu(II) compounds. Also during the backward scan, reduction peaks **c1** and **c2** are seen in the cathodic part. These peaks correspond to the reduction of the insoluble Cu(I) and Cu(II) compounds formed previously during the anodic scan (Fig. 8 c,c'). Anodic peaks **A1** observed at potentials higher than 0.5 V presumably correspond to the Cu(III)/Cu(II) couple which always appears in the course of the oxidation of copper in strongly alkaline solutions. The formal reduction potential of Cu(III)/Cu(II) in a 1 M NaOH solution stands at 0.56 V vs. Ag/AgCl. It should be mentioned that sodium borohydride is inactive at the Cu/Ti electrodes at low potentials. Enhanced anodic currents (peak **A1**) are observed under the potential region of Cu(II)/Cu(III) transition and may be related with the strong interaction of sodium borohydride with the surface already covered by insoluble Cu(II) compounds.

Figure 9 shows positive-going potential stabilized scans (5th cycle) of the oxidation of BH_4^- ions recorded on bare Au, M/Ti, M/TiO₂-NTs, Au(M)/Ti and Au(M)/TiO₂-NTs catalysts with different Au loadings. The oxidation peaks observed at a potential of -0.8 V (peak **A0**) is attributed to the oxidation of H₂, generated by the catalytic hydrolysis of BH_4^- . The current density values are significantly higher in comparison with the current density values obtained using pure Au, Ni/Ti or Ni/TiO₂-NTs electrodes (Fig. 9 a,b). It proves that the prepared Au(Ni)/Ti and Au(Ni)/TiO₂-NTs catalysts have a higher catalytic activity for direct sodium borohydride oxidation. The direct oxidation peak current densities of BH_4^- (peak **A**) for the Au(Ni)/Ti and Au(Ni)/TiO₂-NTs (Fig. 9 a,b) catalysts with different Au

loadings are ca. 10-15 and ~7-13, respectively, times higher as compared to those of the pure Au electrode.

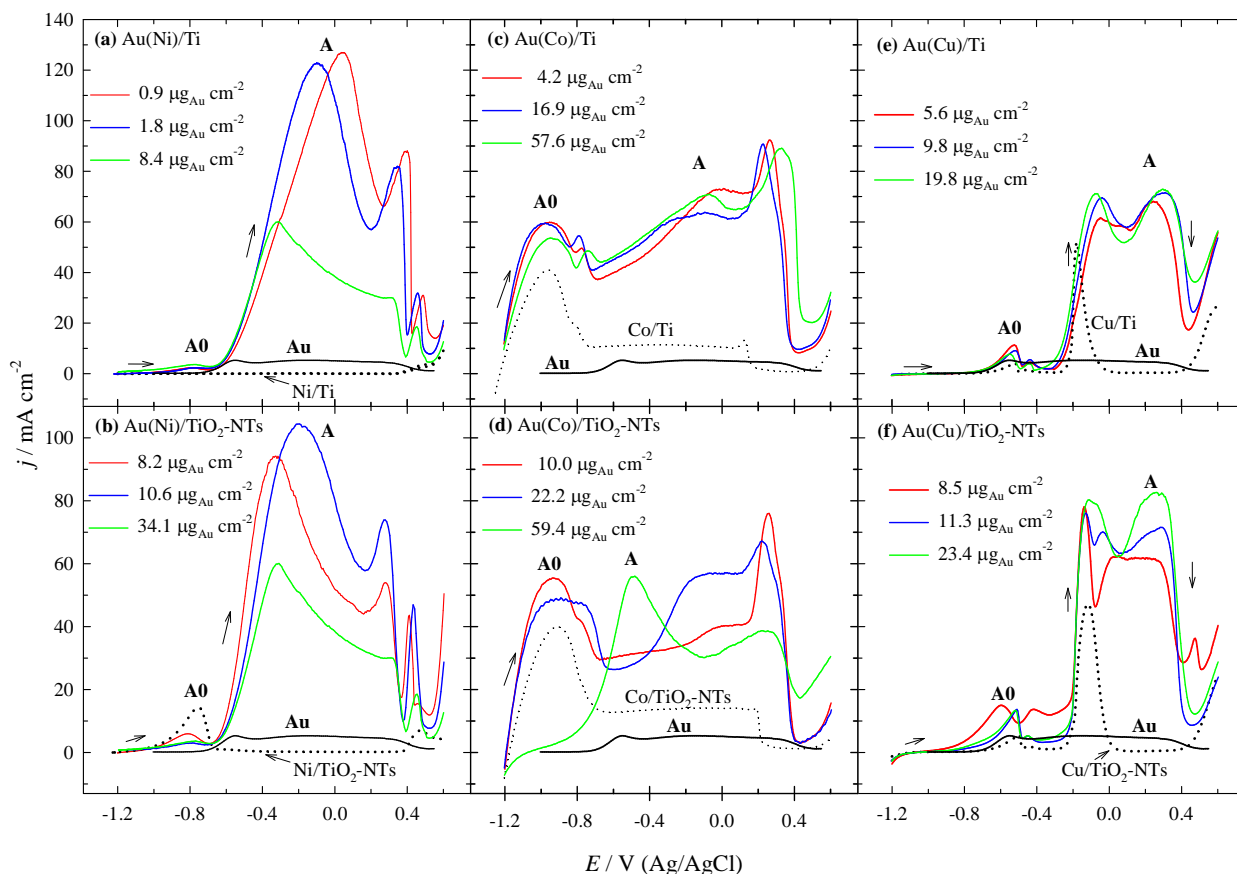


Fig. 9. Positive going scans of BH_4^- oxidation recorded on the Au (a,b), M/Ti, M/TiO₂-NTs, Au(M)/Ti and Au(M)/TiO₂-NTs catalysts with different Au loadings in 0.05 M NaBH₄ + 1 M NaOH at 10 mV s⁻¹; 25 °C.

Once the oxidation of BH_4^- ions on the latter catalysts is compared, it is seen that the highest current densities are observed on the Au(Ni)/Ti catalyst with a lower Au loading of 0.9 $\mu\text{g}_{\text{Au}} \text{cm}^{-2}$ (Fig. 9 a). With increase in Au loading up to 8.4 $\mu\text{g}_{\text{Au}} \text{cm}^{-2}$ on the Ni/Ti electrode the potential values of peak **A** are shifted to negative potential values. To compare the electrocatalytic activity of these catalysts, the current density was normalized in reference to the Au loadings for each catalyst to represent the mass activity of catalysts towards the oxidation of sodium borohydride.

The Au mass peak current (peak **A**) of the Au(Ni)/Ti catalyst with the Au loading of $0.9 \mu\text{g}_{\text{Au}}\text{cm}^{-2}$ is 2.1-14.3 times higher than those on the Au(Ni)/Ti catalysts with the Au loadings of 1.8 and $8.4 \mu\text{g}_{\text{Au}}\text{cm}^{-2}$, respectively. The Au mass peak current (peak **A**) of the Au(Ni)/TiO₂-NTs catalyst with the Au loading of $8.2 \mu\text{g}_{\text{Au}}\text{cm}^{-2}$ is 1.2-6.5 times higher than those on the Au(Ni)/TiO₂-NTs catalysts with the Au loadings of 10.6 and $34.1 \mu\text{g}_{\text{Au}}\text{cm}^{-2}$, respectively. The higher mass specific current density have been obtained on the Ti surface. The Au mass peak current (peak **A**) of the Au(Ni)/Ti catalyst with the Au loading of $0.9 \mu\text{g}_{\text{Au}}\text{cm}^{-2}$ is 12.2 times higher than those on the Au(Ni)/TiO₂-NTs catalyst with the Au loading of $8.2 \mu\text{g}_{\text{Au}}\text{cm}^{-2}$.

The electrochemical behavior of the Co/Ti, Co/TiO₂-NTs, Au(Co)/Ti and Au(Co)/TiO₂-NTs catalysts towards the oxidation of BH₄⁻ ions was also evaluated in an alkaline medium using the cyclic voltammetry method (Fig. 9 c,d). During the anodic scan in contrast to the oxidation of BH₄⁻ on the bare Au electrode (Fig. 7), two well-expressed anodic peaks: peak **A0** at lower potential values and peak **A** at more positive potential values are seen in the anodic scans for the as-prepared Co/Ti, Co/TiO₂-NTs, Au(Co)/Ti and Au(Co)/TiO₂-NTs catalysts (Fig. 9 c,d). Oxidation peak **A** that is related to the direct oxidation of BH₄⁻ ions recorded on the Au(Co)/Ti and Au(Co)/TiO₂-NTs catalysts appears in the same potential region as on the pure Au electrode indicating a high activity of the latter catalysts. It should be noted that the both oxidation peaks recorded on the Au(Co)/Ti and Au(Co)/TiO₂-NTs catalysts are higher than those recorded on Co/Ti or Co/TiO₂-NTs. An enhanced electrocatalytic activity of the as-prepared Au(Co)/Ti and Au(Co)/TiO₂-NTs catalysts can be ascribed to the intrinsic electrocatalytic activity of the Au nanoparticles deposited on the Co/Ti surface and formation of AuCo alloy as was confirmed by XRD analysis (Fig. 6 c). Wide oxidation waves recorded both on bare Au and the Au(Co)/Ti catalysts, which extend up to 0.4 V, correspond to the oxidation of the reaction intermediates on the partially oxidized Au surface. It can be noted that the Au(Co)/TiO₂-NTs electrode with the Au loading of $59 \mu\text{g}_{\text{Au}}\text{cm}^{-2}$ and the bare Au electrode has the same potential value of oxidation peak **A** (ca. -0.5 V, Fig. 9 d), the peak current

density being ca. 7 times higher than that of pure Au. Additionally, the Au(Co)/TiO₂-NTs electrode with the highest Au loading of 59 μg_{Au}cm⁻² shows an almost negligible anodic peak **A0**, probably as a result of the lower Co content on the surface of this electrode (Table IV). Furthermore, the CV profile of Au(Co)/TiO₂-NTs (59 μg_{Au}cm⁻²) in the potential region from ca. -0.7 V to 0.4 V (Fig. 9 d) showed characteristics similar to that of pure Au in the alkaline borohydride solution (Fig. 7). It is worth noting that this potential region is in the vicinity of that of Au monolayer formation on the Co/TiO₂-NTs surface. It is clear that the Au mass specific peak current density of the Au(Co)/TiO₂-NTs catalyst with the Au loading of 10 μg_{Au}cm⁻² is higher than that of the Au(Co)/TiO₂-NTs catalysts with the Au loadings of 22 and 59 μg_{Au}cm⁻², respectively. The Au mass peak current (peak **A**) of the Au(Co)/Ti catalyst with the Au loading of 4.2 μg_{Au}cm⁻² is 4-14 times higher than those on the Au(Co)/Ti catalysts with the Au loadings of 16.9 and 57.6 μg_{Au}cm⁻², respectively. This phenomenon could be explained by the size of Au nanoparticles, i.e. when the Au loading on the Co/Ti or Co/TiO₂-NTs is the lowest, the size of Au nanoparticles is also the smallest one compared with higher Au loadings deposited on the Co/Ti or Co/TiO₂-NTs surfaces (Fig. 4). Mass specific peak current density is ca. 3.2 times higher using Au(Co)/Ti catalyst with the Au loading of 4.2 μg_{Au}cm⁻² than that of the Au(Co)/TiO₂-NTs catalyst with the Au loading of 10 μg_{Au}cm⁻².

Figure 9 (e and f) shows stabilized anodic scans (5th cycles) of the oxidation of BH₄⁻ ions recorded on Cu/Ti, Cu/TiO₂-NTs and different Au(Cu)/Ti and Au(Cu)/TiO₂-NTs catalysts. Since the Cu/Ti or Cu/TiO₂-NTs electrodes do not show electroactivity towards the direct electrooxidation of BH₄⁻ ions (Fig. 9 e,f), the observed prominent anodic currents under the potential region of -0.4 and 0.5 V can be ascribed to the electrocatalytic activity of Au nanoparticles deposited on the Cu/Ti or Cu/TiO₂-NTs electrodes. Noteworthy, the current densities of peak **A** on the Au(Cu)/Ti and Au(Cu)/TiO₂-NTs catalysts are ca. 7.7-8.9 and 10-fold, respectively, higher compared to those on pure Au.

The Au mass peak current (peak **A**) of the Au(Cu)/Ti catalyst with the Au loading of 5.6 μg_{Au}cm⁻² is ca. 1.5-3 times higher than those on the Au(Cu)/Ti catalysts with the Au loadings of 9.8 and 19.8 μg_{Au}cm⁻², respectively. The Au mass peak current (peak **A**) of the

Au(Cu)/TiO₂-NTs catalyst with the Au loading of 8.5 μg_{Au}cm⁻² is ca. 1.4-2.7 times higher than those on the Au(Cu)/TiO₂-NTs catalysts with the Au loadings of 11.3 and 23.4 μg_{Au}cm⁻², respectively. A higher mass specific current density was obtained on the Ti surface. The Au mass peak current (peak A) of the Au(Cu)/Ti catalyst with the Au loading of 5.6 μg_{Au}cm⁻² is ca. 1.2 times higher than that on the Au(Cu)/TiO₂-NTs catalyst with the Au loading of 8.5 μg_{Au}cm⁻².

The current density of the Au(Ni)/Ti catalyst with the Au loading of 0.9 μg_{Au}cm⁻² is 1.3 and 2.0 times higher than those on the Au(Co)/Ti and Au(Cu)/Ti catalysts with the Au loadings of 4.2 and 5.6 μg_{Au}cm⁻², respectively. The current density of the Au(Ni)/TiO₂-NTs catalyst with the Au loading of 8.2 μg_{Au}cm⁻² is 1.2 and 1.5 times higher than those on the Au(Co)/TiO₂-NTs and Au(Cu)/TiO₂-NTs catalysts with the Au loadings of 10.0 and 8.5 μg_{Au}cm⁻², respectively.

Au(M)/Ti and Au(Cu)/TiO₂-NTs (M = Ni, Co, Cu) catalysts have an enhanced electrocatalytic activity towards the oxidation of sodium borohydride as compared with that of pure Au, M/Ti and M/TiO₂-NTs. The highest catalytic activity was obtained using the catalysts with a Ni sublayer deposited on the Ti or TiO₂-NTs surfaces. The fabricated Au(M)/Ti and Au(M)/TiO₂-NTs catalysts seem to be a promising anodic material for direct borohydride fuel cells.

3.3. NaBH₄-H₂O₂ fuel cell test experiments

Direct alkaline NaBH₄-H₂O₂ single fuel cell tests were carried out by employing the prepared M/Ti, M/TiO₂-NTs, Au(M)/Ti and Au(M)/TiO₂-NTs catalysts (with a geometric area of 2 cm²) as the anode and a Pt sheet as the cathode. The anolyte was composed of an alkaline mixture of 1 M NaBH₄ + 4 M NaOH and the catholyte contained 5 M H₂O₂ + 1.5 M HCl at temperatures of 25-55 °C. The performance of the fuel cell was evaluated by recording the cell polarization and obtaining the corresponding power density curves. Figure 10 presents the fuel cell polarization curves and the corresponding power densities against the current density by employing the M/Ti, M/TiO₂-NTs, Au(M)/Ti and Au(M)/TiO₂-NTs catalysts at a temperature of 25 °C. Notably, peak power density values increase with the

increase in DBHPFC temperature and are greater when using Au(M)/Ti or Au(M)/TiO₂-NTs catalysts as anode material as compared with those of M/Ti or M/TiO₂-NTs. During the cell discharge process, small bubbles of hydrogen and oxygen were observed at the electrodes surface due to the chemical decomposition of BH₄⁻ and H₂O₂ at the anode and at the cathode, respectively. The fuel cell displayed an open circuit voltage of ca. 1.9 V using catalysts with a Ni or Co sublayer on the Ti and TiO₂-NTs surfaces and ca. 1.6 V using catalysts with a Cu sublayer on the Ti and TiO₂-NTs surfaces.

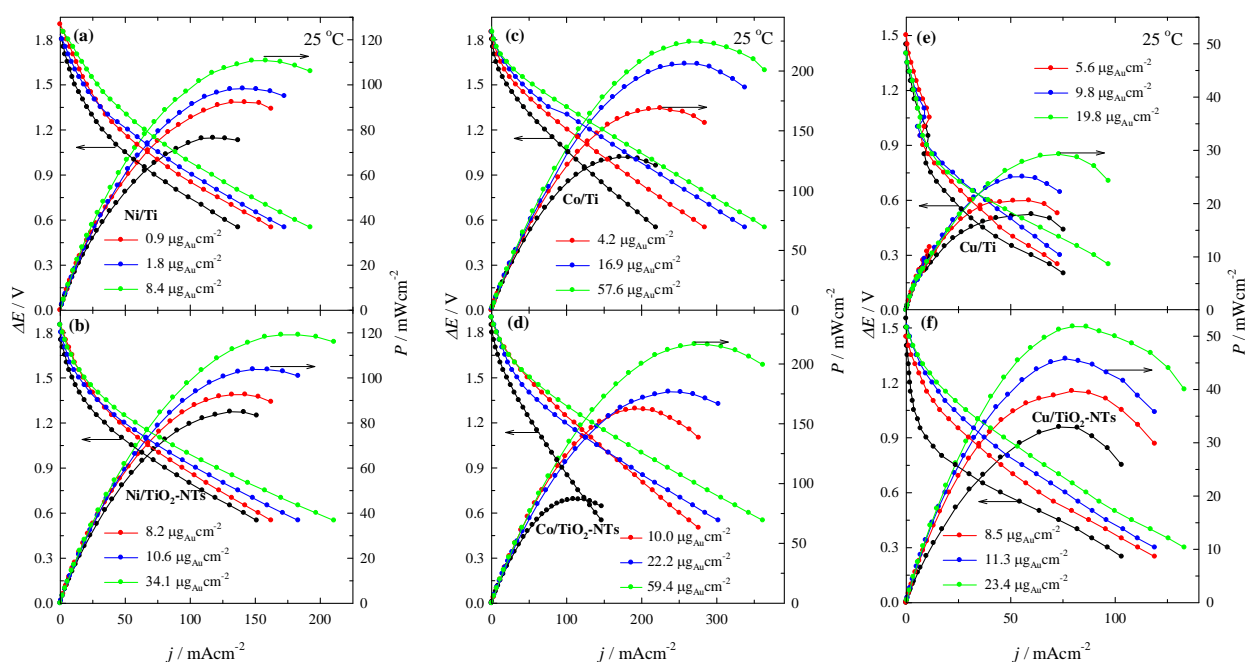


Fig. 10. Cell polarization and power density curves for the DBHPFC using M/Ti, M/TiO₂-NTs, Au(M)/Ti and Au(M)/TiO₂-NTs anode catalysts with anolyte consisted of 1 M NaBH₄ + 4 M NaOH and 5 M H₂O₂ + 1.5 M HCl catholyte at 25 °C.

As seen, the M/Ti and M/TiO₂-NTs electrodes generate the maximum power density of ca. 18-128 and 33-87 mW cm⁻², respectively, at 25 °C. Peak power densities up to 128 mW cm⁻² were attained at 25 °C at a current density of 171 mA cm⁻² and a cell voltage of 0.75 V using the Co/Ti electrode (Table V) and it is ~1.7 and 7.1 times higher than the power densities obtained using Ni/Ti and Cu/Ti electrodes under the same conditions (Table V). Peak power densities up to 87 mW cm⁻² were attained at 25 °C at a current density of 109 mA cm⁻² and a cell voltage of 0.8 V using the Co/TiO₂-NTs electrode and it

is ~1 and 2.6 times higher than the power densities obtained using Ni/TiO₂-NTs and Cu/TiO₂-NTs electrodes under the same conditions (Table V). The peak power densities are 1.5-1.7 times higher with a Co sublayer on the Ti surface than those on the TiO₂-NTs surface at temperatures of 25-55 °C.

The electrochemical parameters of DBHPFCs using different Au(M)/Ti and Au(M)/TiO₂-NTs anode catalysts are shown in Tables VI-VIII. The Au(Ni)/Ti and Au(Ni)/TiO₂-NTs generate the maximum power density of ca. 92-162 and 93-167 mW cm⁻², respectively, at temperatures of 25-55 °C. Peak power densities up to 93 mW cm⁻² were attained at 25 °C at a current density of 142 mA cm⁻² and a cell voltage of 0.65 V using the Au(Ni)/TiO₂-NTs catalyst with the Au loading of 8.2 μg_{Au}cm⁻² (Table VI). The Au(Co)/Ti and Au(Co)/TiO₂-NTs generate the maximum power density of ca. 169-288 and 163-283 mW cm⁻², respectively, at temperatures of 25-55 °C. Peak power densities up to 169 mW cm⁻² were attained at 25 °C at a current density of 225 mA cm⁻² and a cell voltage of 0.75 V using the Au(Co)/Ti catalyst with the Au loading of 4.2 μg_{Au}cm⁻² (Table VII). The Au(Cu)/Ti and Au(Cu)/TiO₂-NTs generate a peak power density of ca. 21-38 and 40-92 mW cm⁻², respectively, at temperatures of 25-55 °C.

TABLE V. Electrochemical parameters of DBHPFCs using the M/Ti, M/TiO₂-NTs (M=Ni, Co, Cu) anode catalysts.

Catalyst	T (°C)	Peak power density (mW cm⁻²)	<i>j</i> at peak power density (mA cm⁻²)	<i>E</i> at peak power density (V)
Ni/Ti	25	76.4	117.5	0.65
	35	92.4	131.9	0.70
	45	103.3	147.5	0.70
	55	109.3	128.4	0.85
Ni/TiO ₂ -NTs	25	85.0	130.6	0.65
	35	92.7	142.5	0.65
	45	106.5	163.7	0.65
	55	120.8	172.5	0.70
Co/Ti	25	128.0	170.6	0.75
	35	141.6	188.7	0.75
	45	157.1	209.3	0.75
	55	177.1	221.2	0.80
Co/TiO ₂ -NTs	25	87.0	108.7	0.80
	35	89.1	118.7	0.75
	45	94.2	125.6	0.75
	55	101.7	135.6	0.75
Cu/Ti	25	18.0	60.0	0.30
	35	22.7	64.7	0.35
	45	24.6	61.4	0.40
	55	27.0	67.5	0.40
Cu/TiO ₂ -NTs	25	33.0	73.2	0.45
	35	41.2	82.3	0.50
	45	44.4	80.6	0.55
	55	54.9	84.4	0.65

TABLE VI. Electrochemical parameters of DBHPFCs using different Au(Ni)/Ti, Au(Ni)/TiO₂-NTs anode catalysts.

Catalyst	Au loading ($\mu\text{g}_{\text{Au}}\text{cm}^{-2}$)	T (°C)	Peak power density (mW cm^{-2})	<i>j</i> at peak power density (mA cm^{-2})	<i>E</i> at peak power density (V)	Specific peak power density ($\text{mW } \mu\text{g}_{\text{Au}}^{-1}$)
Au(Ni)/Ti	0.9	25	92.3	131.8	0.70	102.6
		35	104.2	148.7	0.70	115.8
		45	114.3	163.1	0.70	127.0
		55	123.5	176.2	0.70	137.2
	1.8	25	98.3	140.4	0.70	54.6
		35	113.4	174.3	0.65	63.0
		45	128.2	197.2	0.65	71.2
		55	134.9	192.5	0.70	74.9
	8.4	25	110.7	158.1	0.70	13.2
		35	128.2	197.2	0.65	15.3
		45	143.1	220.0	0.65	17.0
		55	161.8	215.6	0.75	19.3
Au(Ni)/TiO ₂ -NTs	8.2	25	92.6	142.3	0.65	11.3
		35	108.1	166.2	0.65	13.2
		45	122.8	175.3	0.70	15.0
		55	131.1	187.2	0.70	16.0
	10.6	25	103.8	148.1	0.70	9.8
		35	119.5	170.6	0.70	11.3
		45	130.2	185.9	0.70	12.3
		55	147.0	195.9	0.75	13.9
	34.1	25	119.1	183.1	0.65	3.5
		35	135.1	180.0	0.75	4.0
		45	149.3	186.5	0.80	4.4
		55	166.9	196.2	0.85	4.9

TABLE VII. Electrochemical parameters of DBHPFCs using different Au(Co)/Ti, Au(Co)/TiO₂-NTs anode catalysts.

Catalyst	Au loading ($\mu\text{g}_{\text{Au}}\text{cm}^{-2}$)	T (°C)	Peak power density (mW cm^{-2})	<i>j</i> at peak power density (mA cm^{-2})	<i>E</i> at peak power density (V)	Specific peak power density ($\text{mW } \mu\text{g}_{\text{Au}}^{-1}$)	
Au(Co)/Ti	4.2	25	168.8	225.0	0.75	40.2	
		35	182.3	214.3	0.85	43.4	
		45	195.1	229.3	0.85	46.5	
		55	200.6	250.6	0.80	47.8	
	16.9	25	206.1	257.5	0.80	12.2	
		35	228.6	285.6	0.80	13.5	
		45	244.6	305.6	0.80	14.5	
		55	259.9	305.6	0.85	15.4	
	57.6	25	224.3	263.7	0.85	3.9	
		35	256.2	301.2	0.85	4.5	
		45	277.5	326.2	0.85	4.8	
		55	288.1	338.7	0.85	5.0	
	Au(Co)/TiO ₂ -NTs	10.0	25	162.6	191.2	0.85	16.3
			35	178.0	209.3	0.85	17.8
			45	191.5	239.3	0.8	19.2
			55	204.0	254.9	0.8	20.4
22.2		25	176.8	235.6	0.75	8.0	
		35	189.5	252.4	0.75	8.5	
		45	218.1	272.4	0.8	9.8	
		55	258.1	322.4	0.8	11.6	
59.4		25	216.6	270.6	0.8	3.7	
		35	239.1	298.7	0.8	4.0	
		45	262.0	308.0	0.85	4.4	
		55	283.3	333.0	0.85	4.8	

TABLE VIII. Electrochemical parameters of DBHPFCs using different Au(Cu)/Ti, Au(Cu)/TiO₂-NTs anode catalysts.

Catalyst	Au loading ($\mu\text{g}_{\text{Au}}\text{cm}^{-2}$)	T ($^{\circ}\text{C}$)	Peak power density (mW cm^{-2})	j at peak power density (mA cm^{-2})	E at peak power density (V)	Specific peak power density ($\text{mW } \mu\text{g}_{\text{Au}}^{-1}$)	
Au(Cu)/Ti	5.6	25	20.6	58.7	0.35	3.7	
		35	23.8	59.4	0.40	4.3	
		45	26.6	66.4	0.40	4.8	
		55	29.4	73.5	0.40	5.3	
	9.8	25	25.1	55.6	0.45	2.6	
		35	27.2	60.4	0.45	2.8	
		45	29.4	73.4	0.40	3.0	
		55	33.7	84.1	0.40	3.4	
	19.8	25	29.3	73.1	0.40	1.5	
		35	31.7	79.1	0.40	1.6	
		45	34.1	85.1	0.40	1.7	
		55	38.0	94.8	0.40	1.9	
	Au(Cu)/TiO ₂ -NTs	8.5	25	39.7	79.3	0.50	4.7
			35	45.3	90.5	0.50	5.3
			45	51.3	93.1	0.55	6.0
			55	62.6	89.4	0.70	7.4
11.3		25	45.8	76.2	0.60	4.1	
		35	54.7	99.4	0.55	4.8	
		45	62.6	104.3	0.60	5.5	
		55	71.7	119.5	0.60	6.3	
23.4		25	51.8	79.7	0.65	2.2	
		35	63.8	98.1	0.65	2.7	
		45	80.8	134.7	0.60	3.5	
		55	91.9	153.1	0.60	3.9	

Peak power densities up to 40 mW cm^{-2} were attained at $25 \text{ }^{\circ}\text{C}$ at a current density of 79 mA cm^{-2} and a cell voltage of 0.5 V using the Au(Cu)/TiO₂-NTs catalyst with the Au loading of $8.5 \mu\text{g}_{\text{Au}}\text{cm}^{-2}$ (Table VIII). Peak power density is 1.8 and 8.2 times higher at $25 \text{ }^{\circ}\text{C}$ using the Au(Co)/Ti catalyst after immersion into the gold-containing solution for

0.5 min than using the Au(Ni)/Ti and Au(Cu)/Ti catalysts, respectively, under the same conditions. Peak power density is 1.8 and 4.1 times higher at 25 °C using the Au(Co)/TiO₂-NTs catalyst after immersion into the gold-containing solution for 0.5 min than Au(Ni)/TiO₂-NTs and Au(Cu)/TiO₂-NTs catalysts, respectively, under the same conditions.

To compare the catalytic activity of the Au(M)/Ti and Au(M)/TiO₂-NTs catalysts, the peak power density values were normalized in reference to the Au loadings for each catalyst, i.e. the power density per microgram of Au and are given in Tables VI-VIII. It is clear that the Au specific peak power density of the Au(M)/Ti and Au(M)/TiO₂-NTs catalysts with the lowest Au loadings is higher than that of the catalysts with higher Au loadings. The highest specific peak power densities of 102.6 mW μg_{Au}⁻¹ at 25 °C were attained using the Au(Ni)/Ti anode with the Au loading of 0.9 μg cm⁻² and of 16.3 mW μg_{Au}⁻¹ at 25 °C were attained using the Au(Ni)/TiO₂-NTs anode with the Au loading of 10.0 μg cm⁻².

Direct alkaline NaBH₄-H₂O₂ single fuel cell tests were carried out by employing the prepared M/Ti, M/TiO₂-NTs, Au(M)/Ti and Au(M)/TiO₂-NTs catalysts at temperatures of 25-55 °C. It was found that the highest peak power densities up to 224 mW cm⁻² were attained at 25 °C using the Au(Co)/Ti catalyst, with the Au loading of 57.6 μg cm⁻². The highest specific peak power densities of 102.6 mW μg_{Au}⁻¹ at 25 °C were attained using the Au(Ni)/Ti anode with the Au loading of 0.9 μg cm⁻².

CONCLUSIONS

1. The Au(M)/Ti and Au(M)/TiO₂-NTs (M = Ni, Cu, Co) catalysts were prepared by means of the electroless metal deposition and galvanic displacement techniques. It has been found that:

a) with the aim of formation of effective catalysts, the immobilization of Au nanoparticles should be made on the underlayers deposited on the Ti and TiO₂-NTs surfaces with the thickness of ca. 0.2-0.4 μm for Ni, ca. 0.5-1.1 μm for Co and ca. 1.5 μm for Cu;

b) the optimal time period of immersion for Au deposition varies from 0.5 to 5 minutes. Due to spontaneous displacement of metal by gold, the Au(M)/Ti Au(M)/TiO₂-NTs catalysts were fabricated with the Au nanoparticles sized ca. 10-100 nm and having the Au loadings from ca. 0.9 to 59.4 μg_{Au} cm⁻².

2. The prepared Au(M)/Ti and Au(M)/TiO₂-NTs catalysts have a significantly higher electrocatalytic activity towards the oxidation of sodium borohydride as compared to that of the bare Au, M/Ti and M/TiO₂-NTs electrodes. The Au(M)/Ti catalysts with the Au loading from 0.9 to 57.6 μg_{Au} cm⁻², and the Au(M)/TiO₂-NTs catalysts with the Au loading from 8.2 to 59.4 μg_{Au} cm⁻² exhibit ca. 7-16 times higher electrocatalytic activity towards the electrooxidation reaction of sodium borohydride in an alkaline medium as compared with that of bare Au electrode. The highest mass activity (140 mA μg_{Au}⁻¹) towards the oxidation reaction of sodium borohydride was obtained on the Au(Ni)/Ti catalyst with the Au loading of 0.9 μg_{Au} cm⁻².

3. Direct alkaline NaBH₄-H₂O₂ single fuel cell tests were carried out by employing the prepared M/Ti, M/TiO₂-NTs, Au(M)/Ti and Au(M)/TiO₂-NTs catalysts as the anodes. It has been found that the highest peak power density up to 224 mW cm⁻² was attained at a temperature of 25 °C using the Au(Co)/Ti catalyst with the Au loading of 57.6 μg cm⁻² as the anode. The highest specific peak power density of 102.6 mW μg_{Au}⁻¹ at a temperature of 25 °C was attained using Au(Ni)/Ti with the Au loading of 0.9 μg cm⁻² as an anode.

4. The Au(M)/Ti and Au(M)/TiO₂-NTs catalysts are promising materials and can be used as anodes in direct sodium borohydride fuel cells.

List of Publications

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2. D. M. F. Santos, **A. Balčiūnaitė**, L. Tamašauskaitė-Tamašiūnaitė, A. Zabielaitytė, A. Jagminienė, I. Stankevičienė, A. Naujokaitis, E. Norkus. “*AuCo/TiO₂-NTs anode catalysts for direct borohydride fuel cells*“. J. Electrochem. Soc. 163(14) (2016) F1553-F1557.
3. L. Tamašauskaitė-Tamašiūnaitė, J. Rakauskas, **A. Balčiūnaitė**, A. Zabielaitytė, J. Vaičiūnienė, A. Selskis, E. Norkus. “*Nanostructured gold-nickel/titania nanotubes electrocatalysts for hydrazine oxidation*“. J. Power Sources 272 (2014) 362-370.
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5. L. Tamašauskaitė-Tamašiūnaitė, A. Jagminienė, **A. Balčiūnaitė**, A. Zabielaitytė, A. Žielienė, L. Naruškevičius, J. Vaičiūnienė, A. Selskis, R. Juškėnas, E. Norkus. “*Electrocatalytic activity of the nanostructured Au-Co catalyst deposited onto titanium towards borohydride oxidation*“. Int. J. Hydrogen Energy 38 (2013) 14232-14241.
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Awards

2013 - Laureate of the Conference of Young Researchers, organized by Lithuanian Academy of Sciences.

2013 - INFOBALT award for the study “*Investigation of borohydride oxidation at the nanostructured Au-Cu deposited on the titania nanotube arrayed surface*”.

2013 - Lithuanian Academy of Sciences award for the best student study “*Investigation of borohydride oxidation at the nanostructured Au(Ni)/TiO₂-NTs electrode*”.

NAUJOS MEDŽIAGOS ŠARMINIAMS KURO ELEMENTAMS: SINTEZĖ, CHARAKTERIZAVIMAS IR SAVYBĖS

Santrauka

Alternatyvių energijos šaltinių paiešką lemia didėjantis energijos poreikis bei senkantys tradiciniai energijos šaltiniai bei resursai. Kuro elementas cheminės reakcijos energiją tiesiogiai verčia elektros energija. Kuro elementai kol kas yra švariausias žinomas elektros energijos gavimo būdas. Disertacinis darbas susietas su perspektyviais, visame pasaulyje intensyviai vykdomais kuro elementuose naudojamų medžiagų savybių tyrimais ir yra skirtas naujų efektyvių medžiagų paieškai, kurias galima pritaikyti tiesioginių natrio borohidrido kuro elementų sukūrimui, siekiant padidinti esamų ar naujų kuro elementų našumą. Taigi šio darbo tikslas buvo efektyvių katalizatorių formavimas, apibūdinimas bei taikymas tiesioginiuose natrio borohidrido kuro elementuose.

Šio darbo metu buvo formuojami daugiafunkciniai M/Ti, M/TiO₂nv, Au(M)/Ti ir Au(M)/TiO₂nv (M = Ni, Co, Cu) katalizatoriai, taikant paprastus bei santykinai nebrangius cheminio metalų nusodinimo ir galvaninio pakeitimo metodus. Nustatyta, kad efektyvių katalizatorių formavimui, Au nanodalelių imobilizavimui ant Ti ir TiO₂nv paviršiaus, turi būti nusodinamas apie 0,2-0,4 μm storio Ni pasluoksnis, ~0,5-1,1 μm storio Co pasluoksnis ir apie 1,5 μm storio Cu pasluoksnis, o optimalus imersinio Au nusodinimo laikas – 0,5-5 min. Nusodinto Au nanodalelių dydis yra nuo 10-100 nm, o nusodinto Au įkrova yra 0,9-59,4 μg_{Au} cm⁻² suformuotuose Au(M)/Ti bei Au(M)/TiO₂nv katalizatoriuose. Sukurti Au(M)/Ti ir Au(M)/TiO₂nv katalizatoriai pasižymi itin dideliu elektrokataliziniu aktyvumu natrio borohidrido oksidacijos reakcijai, palyginus su jų elektrokataliziniu aktyvumu ant gryno Au, M/Ti ir M/TiO₂nv elektrodų. Natrio borohidrido oksidacijos srovės tankio vertės, išmatuotos ant Au(M)/Ti su nusodinto Au įkrova nuo 0,9 iki 57,6 μg_{Au} cm⁻² ir Au(M)/TiO₂nv katalizatorių su nusodinto Au įkrova nuo 8,2 iki 59,4 μg_{Au} cm⁻² yra apie 7-16 kartų yra didesnės nei ant gryno Au elektrodo. Didžiausiu masės aktyvumu (140 mA μg_{Au}⁻¹) natrio borohidrido oksidacijos reakcijai pasižymėjo Au(Ni)/Ti katalizatorius, su nusodinto Au kiekiu 0,9 μg_{Au} cm⁻². Taip pat nustatyta, kad išmatuotas

didžiausias $\text{NaBH}_4\text{-H}_2\text{O}_2$ kuro elemente prototipo galios tankis $25\text{ }^\circ\text{C}$ temperatūroje yra $224,3\text{ mW cm}^{-2}$, panaudojant $\text{Au}(\text{Co})/\text{Ti}$ katalizatorių su nusodinto Au įkrova $57,6\text{ }\mu\text{g cm}^{-2}$, o specifinis galingumas yra $102,6\text{ mW }\mu\text{g}_{\text{Au}}^{-1}$, panaudojus kaip anodą $\text{Au}(\text{Ni})/\text{Ti}$ katalizatorių su nusodinto Au įkrova $0,9\text{ }\mu\text{g cm}^{-2}$.

Suformuoti $\text{Au}(\text{M})/\text{Ti}$ ir $\text{Au}(\text{M})/\text{TiO}_2\text{nv}$ katalizatoriai yra perspektyvios medžiagos ir gali būti naudojamos kaip anodas tiesioginiuose natrio borohidrido kuro elementuose.

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